

Thermomechanics		
i Calculation without errors.	?	
ii Project information		
Calculations section		
1.0 Calculation units, units conversion		
1.1 Calculation units	SI Units (N, mm, kW,...)	
1.2 Units conversion		
Length	1 m ▼	39.37007874 inch ▼
Area	1 m ² ▼	10.76391042 feet ² ▼
Volume	1 m ³ ▼	35.31466672 feet ³ ▼
Density	1 kg/m ³ ▼	0.062427961 lb/ft ³ ▼
Mass	1 kg ▼	2.204624 lb ▼
Kin.viscosity	1 cSt ▼	0.038750678 ft ² /h ▼
Dyn.viscosity	1 Poise ▼	0.002088555 Slug/(ft·s) ▼
Temperature	20 °C ▼	68 °F ▼
Flow rate	1 m ³ /s ▼	1 m ³ /s ▼
Speed	1 m/s ▼	3.6 km/h ▼
Acceleration	1 m/s ² ▼	3.280839895 ft/s ² ▼
Revolutions	1 /s ▼	6.283185307 rad/sec ▼
Force	1 N ▼	0.224809 lbf ▼
Moment	1 Nm ▼	0.737561 lbf·ft ▼
Pressure	1 Atm ▼	14.22321814 psi ▼
Power	1 W ▼	3.41442595 BTu/h ▼
Energy	1 kWh ▼	3412.12407 BTU ▼
Specific heat capacity	1 J/kg/K ▼	0.000238846 BTU/lb/R ▼
Thermal conductivity	1 W/m/K ▼	0.578175982 BTU/ft/h/ft ² ▼
Heat Transfer Coeff.	1 W/m ² /K ▼	0.176228039 BTu/h/ft ² /°F ▼
Heat Flux Density	1 W/m ² ▼	0.317210472 BTU/h/ft ² ▼
Thermal resistance	1 m ² ·K/W ▼	5.674465912 h·ft ² ·°F/Btu ▼
Heating value	1 J/kg ▼	0.000429923 BTu/lb ▼

2.0 Energy: Temperature change, phase change, fuel heating value

2.1 Energy for temperature change for various materials

2.2 Material group	7. Liquids (L)
2.3 Material	102-L. Water at 10°C ($\rho=1000$; $\lambda=0.6$; $C_p=4190$)
2.4 Density, Thermal conductivity	Rho, λ 1000 0.6 [kg/m ³], [W/m/K]
2.5 Specific heat capacity	Cp 4190 4190 [J/kg/K] <input checked="" type="checkbox"/>
2.6 Mass of medium	m 1 [kg] <input checked="" type="checkbox"/>
2.7 Temperature change	ΔT 10 [°C] <input checked="" type="checkbox"/>
2.8 Energy	E 0.011638898 [kWh] <input checked="" type="checkbox"/>
2.9 Energy	E 41900 [J] <input checked="" type="checkbox"/>

2.10 Energy for phase change for various materials

2.11 Material	14-G. Nitrogen (N) [TM = -209.9°C, TB = -195.8°C]
2.12 Density, Thermal conductivity	Rho, λ 1.25 0.02598 [kg/m ³], [W/m/K]
2.13 Atomic mass, Specific heat capacity	ma, Cp 14.00686 1040 [AMU], [J/kg/K]
2.14 Melting temperature, Boiling temperature	TM, TB -209.9 -195.8 [°C]
2.15 Specific heat capacity of melting and boiling	CpM, CpB 25.73026 199.3881 [kJ/kg]
2.16 Specific heat capacity of melting and boiling	CpM, CpB 25.73026 199.3881 [kJ/kg] <input checked="" type="checkbox"/>
2.17 Mass of medium	m 1 [kg] <input checked="" type="checkbox"/>
2.18 Energy	EM, EB 0.007147 0.055386 [kWh]
2.19 Energy	EM, EB 25730.26 199388.1 [J]

2.20 Heat of combustion, Fuel heating value (S-solid, L-liquid, G-gas)

2.21 Fuel selection	18-L. Ethanol (100%) (C2H5OH) [HHV = 29.7 MJ/kg]
2.22 Density	Rho 789 [kg/m ³]
2.23 Heating value (Low Heating Value)	LHV 26.7 21066.3 [MJ/kg] / [MJ/m ³]
2.24 Heat of combustion (Higher Heating Value)	HHV 29.7 29.7 [+0 %] [MJ/kg] <input checked="" type="checkbox"/>
2.25 Mass of burned fuel	m 1 [kg]
2.26 Combustion efficiency	η 95 95 % [%]
2.27 Energy	E 28215000 [J]
2.28 Energy	E 7.83750627 [kWh]

3.0 Periodic table of elements, ideal gas state and state change, thermodynamic system

3.1 Calculation of molar mass for elements, compounds, and mixtures

N2+O2+Ar+CO2

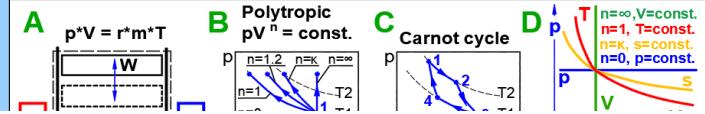
ID	Elements table	Symbol	Number	At.mass	Mol.mass	Density	Spec.Heat	Spec.HeatM	Spec.HeatB	Conduct.	Melting	Boiling	Comp. No.
		Element name	[~]	[~]	[~]	[g/mol]	[kg/m ³]	Cp	CpM	CpB	λ	TM	TB
1	007-G. Nitrogen (N) [Rho = 1.25 kg/m ³] ▼	N	2	14.00686	28.01371	1.25	1040	25.73026	199.3881	0.02598	-209.9	-195.8	1
2	008-G. Oxygen (O) [Rho = 1.43 kg/m ³] ▼	O	2	15.9994	31.9988	1.43	920	13.9124	213.1267	0.02674	-218.4	-183	2
3	018-G. Argon (Ar) [Rho = 1.78 kg/m ³] ▼	Ar	1	39.948	39.948	1.78	520	29.73866	161.3848	0.01772	-189.2	-185.7	3
4	006-S. Carbon (C) [Rho = 2250 kg/m ³] ▼	C	1	12.0106	12.0106	2250	710		29623.83	129	3367	4827	4
5	008-G. Oxygen (O) [Rho = 1.43 kg/m ³] ▼	O	2	15.9994	31.9988	1.43	920	13.9124	213.1267	0.02674	-218.4	-183	4
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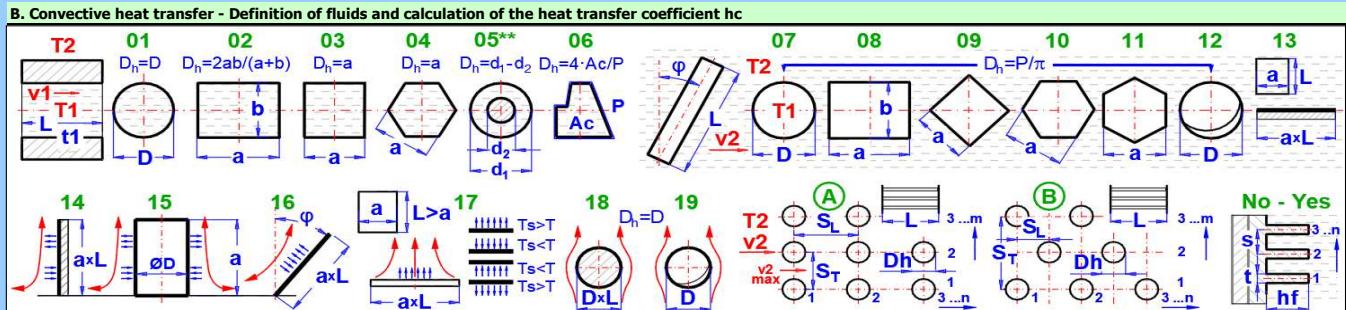
3.5 Mixture parameters

3.6 Serial number	i	1	2	3	4	5	6	7	8	9	10	11	12	Sum
3.7 Poisson's constant	k(i)	1.4	1.4	1.666667	1.333333									[g/mol]
3.8 Molar mass	M(i)	28.0137	31.9988	39.948	44.0094									[%]
3.9 Mass fraction in %	x	75.518	23.135	1.288	0.059									100
3.10 Molar mass	M% _(i)	2.695751	0.722996	0.032242	0.001341									3.45233 [mol]
3.11 Molar mass	Msum	28.96594581		[g/mol]										
3.12 Specific gas constant	r	287.0426767		[J/kg/K]										
3.13 Poisson's constant	k	1.402849608		[~]										

3.14 Equilibrium state and ideal gas state change

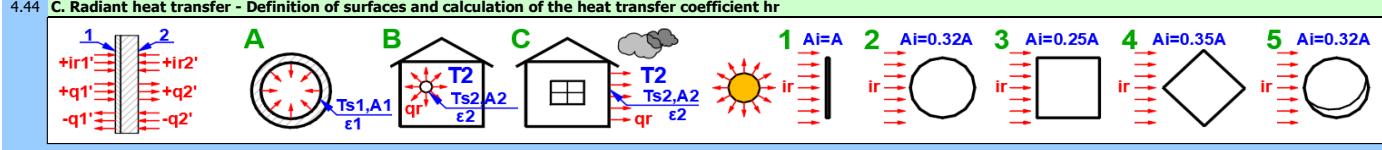
3.15 Gas selection	Tdef	25	92.1	[°C]
3.16 Reference temperature	M	28.96595	28.96595	[kg/kmol]
3.17 Molar mass	r	287.0427	287.0427	[J/kg/K]





4.10 Commonly used combinations of convective heat transfer									
4.11 12. Vertical surface - Free convection (14) <=> Flow across a plate - Forced convection (13)									
4.12 1. Medium - Inner (left) side					2. Medium - Outer (right) side				
4.13 Fluid / Gas	17-G. Air [250...1050K]				Fluid / Gas	17-G. Air [250...1050K]			
4.14 Temperature of the inner (left) side of the wall	Ts1	20.624	20.62374	[°C]	Temperature of the outer (right) side of the wall	Ts2	1.420	1.419794	[°C]
4.15 Definition temperature	Tdef1 = (T1+Ts1)/2	[22.81°C]	22.81187	[°C]	Definition temperature	Tdef2 = (T2+Ts2)/2	[0.71°C]	0.709897	[°C]
4.16 Density	Rho	1.188883	[kg/m³]		Density	Rho	1.284832	[kg/m³]	
4.17 Dynamic viscosity	μs, μ	1.82E-05	1.83E-05	[Pa.s]	Dynamic viscosity	μs, μ	1.73E-05	1.73E-05	[Pa.s]
4.18 Specific heat capacity	Cp	1006.184	[J/kg/K]		Specific heat capacity	Cp	1005.093	[J/kg/K]	
4.19 Thermal conductivity	λ	2.58E-02	[W/m/K]		Thermal conductivity	λ	2.41E-02	[W/m/K]	

4.20 Coefficient of volumetric expansion	β	3.38E-03 [1/K]	Coefficient of volumetric expansion	β	3.65E-03 [1/K]
4.21 Kinematic viscosity	ν	15.42656 [mm ² /s]	Kinematic viscosity	ν	13.44042 [mm ² /s]
Flow type: A-Forced convection, B-Natural convection					
A-14. Vertical surface (Heat Transfer Appl. for the PE) [1e3<Ra<1e13]					
4.24 Flow velocity, Flow rate	v1,m1'	0.001 0.014861 [m/s,kg/s]	Flow velocity, Flow rate	v2,m2'	2 32.12081 [m/s,kg/s]
4.25 Dimension according to the figure	a	2500 1000 [mm] <input checked="" type="checkbox"/>	Dimension according to the figure	a	2500 2500 [mm] <input checked="" type="checkbox"/>
4.26 Dimension according to the figure	L	5000 1000 [mm] <input checked="" type="checkbox"/>	Dimension according to the figure	L	5000 5000 [mm] <input checked="" type="checkbox"/>
4.27 Dimension according to the figure		0 0 [mm] <input checked="" type="checkbox"/>	Dimension according to the figure		0 0 [mm] <input checked="" type="checkbox"/>
4.28 Dimension according to the figure		0 0 [mm] <input checked="" type="checkbox"/>	Dimension according to the figure		0 0 [mm] <input checked="" type="checkbox"/>
Finned surface					
4.30 Finned area	At1	12.905 [m ²]	Finned area	At2	114.29 [m ²]
4.31 Fin efficiency	nφf1	0.978347 [~] <input checked="" type="checkbox"/>	Fin efficiency	nφf2	0.408474 0.408474 [~] <input checked="" type="checkbox"/>
Tube bank					
4.33 Distance between tubes	ST, SL	3183.099 3183.099 [mm] <input checked="" type="checkbox"/>	Not used		
4.34 Number of rows / number of columns	m, n	5 3 [~] <input checked="" type="checkbox"/>			
4.35 Number of tubes in the tube bank	N	1 1 [~] <input checked="" type="checkbox"/>			
4.36 Flow velocity between tubes	v2max	9.319585 9.319585 [m/s] <input checked="" type="checkbox"/>			
4.37 Heat transfer area inner (left)	A1	12.5 12.5 [m ²] <input checked="" type="checkbox"/>			
4.38 Prandtl number	Pr, Prs	0.716095 0.71202 [~] <input checked="" type="checkbox"/>			
4.39 Reynolds number, Critical Re	Re, Recrt	0 1E+09 [~] <input checked="" type="checkbox"/>	Iteration		
4.40 Grashof number, Rayleigh number	Gr, Ra	9.52E+09 6.82E+09 [~] <input checked="" type="checkbox"/>			
4.41 Nusselt number, Characteristic dimension	Nu, a	243.6238 2500 [~], [mm] <input checked="" type="checkbox"/>			
4.42 Convective heat transfer coefficient	hc1	2.511393 2.51128 [W/m ² /K]			
4.43 Heat flux - convection (specific, total)	qc1', Qc1	10.99051 137.3813 [W/m ² , W]			



1. Surface - Inner (left) side					
4.46 Material group	1. Metals and metal alloys (M)				
4.47 Wall material	032-B. Granite: Rough ($\epsilon=0.9$)				
4.48 Emissivity	ϵ_1	0.900	0.900	[~] <input checked="" type="checkbox"/>	
1. Radiation - From inner (left) side					
4.50 Heat radiation into space	A. Not used (closed space..)				
4.51 Radiating area, inner (left)	Ar1	12.5 12.5 [m ²] <input checked="" type="checkbox"/>			
4.52 Radiation heat transfer coefficient	hr1	0 [W/m ² /K]			
4.53 Heat flux - radiation (specific, total)	qr1', Qr1	0 0 [W/m ² , W]			
1. Irradiation - On inner (left) side					
4.55 Incident radiation intensity	ir1'	0 * 1 [W/m ²]			
4.56 Irradiated area size	Ai1	1.25E+01 1.=A [m ²]			
4.57 Radiation heat transfer coefficient	hi1	0 [W/m ² /K]			
4.58 Heat flux - irradiation (\emptyset specific, total)	qi1', Qi1	0 0 [W/m ² , W]			
2. Surface - Outer (right) side					
4.46 Material group	7. Minerals, glass (N)				
4.47 Wall material	045-B. Plaster: Rough ($\epsilon=0.91$)				
4.48 Emissivity	ϵ_2	0.910	0.910	[~] <input checked="" type="checkbox"/>	
2. Radiation - From outer (right) side					
4.50 Heat radiation into space	B. General space radiation				
4.51 Radiating area, outer (right)	Ar2	12.5 12.5 [m ²] <input checked="" type="checkbox"/>			
4.52 Radiation heat transfer coefficient	hr2	4.23937 [W/m ² /K]			
4.53 Heat flux - radiation (specific, total)	qr2', Qr2	6.019031 75.23788 [W/m ² , W]			
2. Irradiation - On outer (right) side					
4.55 Incident radiation intensity	ir2'	0 * ϵ [W/m ²]			
4.56 Irradiated area size	Ai2	12.5 1.=A [m ²]			
4.57 Radiation heat transfer coefficient	hi2	0 [W/m ² /K]			
4.58 Heat flux - irradiation (\emptyset specific, total)	qi2', Qi2	0 0 [W/m ² , W]			

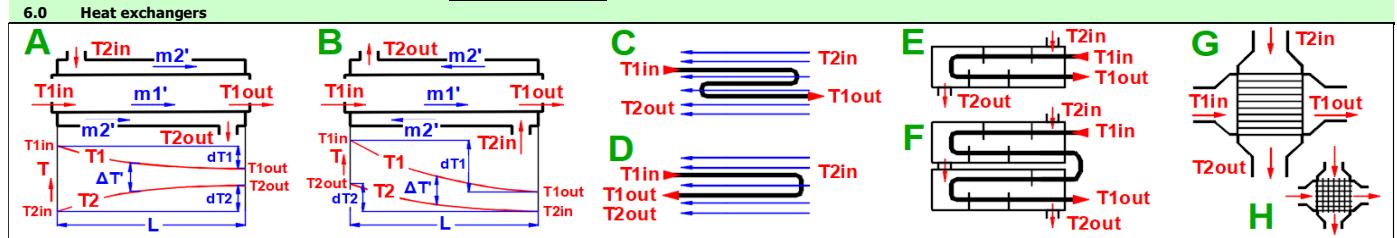
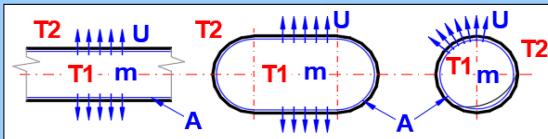
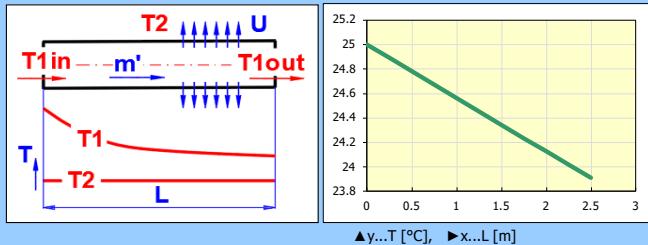
4.59 Heat transfer results					
4.60 Convection + radiation + irradiation					
4.61 Heat transfer coefficient	hc1	2.511393 [W/m ² /K]			
4.62 Heat flux - total (specific, total)	qc1', Qc1	10.99051 137.3813 [W/m ² , W]			
4.63 Overall heat transfer coefficient U, Overall thermal resistance R					
4.64 Inner (left) surface	U1,R1	0.43962 2.274691 [W/m ² /K, m ² K/W]			
4.65 Cylindrical wall	Ucyl1,Rcyl1	1.099051 0.909876 [W/m/K, m.K/W]			
4.66 Spherical wall	Usph1,Rsph1	5.495253 0.181975 [W/K, K/W]			
4.67 Wall thermal resistance (wall only)	Rwall	1.747321 [m ² K/W]			
4.68 Heating / cooling of the working medium					
4.69 Flow area	Af1	1.25E+01 12.5 [m ²] <input checked="" type="checkbox"/>			
4.70 Density	Rho	1.180158 1.180158 [kg/m ³]			
4.71 Specific heat capacity	Cp	1006.314 1006.314 [J/kg/K]			
4.72 Flow rate	m'	0.014752 [kg/s] <input checked="" type="checkbox"/>			
4.73 Inlet / Outlet temperature	Tin1,Tout1	25 17.266 [°C]			
4.74 Heat flux - mean (specific, total)	qs1', Qs1	9.184974 114.8122 [W/m ² , W]			
4.75 Saving the wall heat transfer solution					
4.76 Solution name					
4.77 Structural wall (brick)					
4.78 T1=25 (Air) => 300mm => T2=0 (Air); U1=0.44; q1=11; q2=11					
4.79 Structural wall: Plaster, brick, insulation, plaster					

4a.0 Definition and calculation of finned wall					
1. Fin type - Internal (left) side					
4.81 Thermal conductivity of fin material	λ	0.7 [W/(m.K)]			
4.82 Convective heat transfer coefficient	hc1	2.511393 [W/m ² /K]			
4.83 Wall temperature, medium temperature	Ts1, T1	20.62374 25 [°C]			
4.84 Finned field width	a	50 5000 [mm] <input checked="" type="checkbox"/>			
4.85 Fin profile	A. Rectangle				
4.86 Fin thickness	t	38 38 [mm] <input checked="" type="checkbox"/>			
4.87 Fin height	hf	100 100 [mm]			
2. Fin type - External (right) side					
4.81 Thermal conductivity of fin material	λ	0.7 [W/(m.K)]			
4.82 Convective heat transfer coefficient	hc2	3.501548 [W/m ² /K]			
4.83 Wall temperature, medium temperature	Ts2, T2	1.419794 0 [°C]			
4.84 Finned field width	a	5000 5000 [mm] <input checked="" type="checkbox"/>			
4.85 Fin profile	A. Rectangle				
4.86 Fin thickness	t	3 38 [mm] <input checked="" type="checkbox"/>			
4.87 Fin height	hf	45 100 [mm]			

4a.9 Distance between fins (fin pitch)	s	86	86	[mm]	Distance between fins (fin pitch)	s	10.7	100	[mm]
4a.10 Number of fins in the finned field	n	1	=< 1	[~] <input checked="" type="checkbox"/>	Number of fins in the finned field	n	468	=< 468	[~] <input checked="" type="checkbox"/>
4a.11 Area of one fin / Total area	Af, At	0.595	12.905	[m²] <input checked="" type="checkbox"/>	Area of one fin / Total area	Af, At	0.2325	114.29	[m²] <input checked="" type="checkbox"/>
4a.12 Parameter x, fin efficiency	x, ηf	1.2614	0.5304	[~] <input checked="" type="checkbox"/>	Parameter x, fin efficiency	x, ηf	1.9302	0.3787	[~] <input checked="" type="checkbox"/>
4a.13 Overall finned surface efficiency	ηof	0.9783		[~] <input checked="" type="checkbox"/>	Overall finned surface efficiency	ηof	0.4085		[~] <input checked="" type="checkbox"/>
4a.14 Heat flux - total (specific, overall)	q1', Q1	10.75253	138.7614	[W/m²,W] <input checked="" type="checkbox"/>	Heat flux - total (specific, overall)	q2', Q2	2.03072	232.0909	[W/m²,W] <input checked="" type="checkbox"/>

5.0 Longitudinal temperature change in piping, temperature change and cooling time in the tank (ISO 12241)

5.1 Working fluid	01-L_Water [0...350C]
5.2 Defining temperature	Tdef 25 25 [°C] <input checked="" type="checkbox"/>
5.3 Specific heat capacity	Cp 4187.655 4187.655 [J/kg/K] <input checked="" type="checkbox"/>
5.4 Calculation of longitudinal temperature change in piping	
5.5 Fluid temperature at pipe inlet	T1in 25 25 [°C] <input checked="" type="checkbox"/>
5.6 Ambient temperature	T2 0 0 [°C] <input checked="" type="checkbox"/>
5.7 Mass flow rate through the piping	m' 0.014752 0.014752 [kg/s] <input checked="" type="checkbox"/>
5.8 Heat transfer coefficient (cylinder)	Ucyl 1.099051 1.099051 [W/m/K] <input checked="" type="checkbox"/>
5.9 Distance from the beginning of the pipe	L 2.5 2.5 [m] <input checked="" type="checkbox"/>
5.10 Fluid temperature at point L	T1out 23.9124 [°C] <input checked="" type="checkbox"/>
5.11 Power loss (-) / gain (+)	Pw -0.067185479 [kW] <input checked="" type="checkbox"/>
5.12 Temperature change and cooling time in pipes and tanks	
5.13 Initial fluid temperature	T1s 25 25 [°C] <input checked="" type="checkbox"/>
5.14 Final fluid temperature	T1e 20 0~25 [°C] <input checked="" type="checkbox"/>
5.15 Ambient temperature	T2 0 0 [°C] <input checked="" type="checkbox"/>
5.16 Mass of fluid in the tank	m 0.85 [kg] <input checked="" type="checkbox"/>
5.17 Heat transfer coefficient (area)	U 0.43962 0.43962 [W/m²/K] <input checked="" type="checkbox"/>
5.18 Internal area of the tank or pipe	A 12.5 12.5 [m²] <input checked="" type="checkbox"/>
5.19 Time for cooling / heating	Time 144.54 [s] <input checked="" type="checkbox"/>
5.20 Time for cooling / heating	Time 0:0:2:24.54 [d-h:m:s] <input checked="" type="checkbox"/>
5.21 Energy lost (-) / gained (+)	E -0.004943763 [kWh] <input checked="" type="checkbox"/>



6.0 Heat exchangers

6.1 Heat exchanger type	A. Parallel flow heat exchanger (tube-within-a-tube)
6.2 Load parameters (select from saved wall definitions / current definition)	
6.3 List of defined walls	8 Example 16: Oil/water heat exchanger calculation of heat transfer coefficient U [T1=20 (Water) => 1.5mm] => T2=98 (SAE 10W); U1=41.421; q1=-3231
6.4 Load current parameters from section 4.0 (wall definition)	

6.5 Working fluid 1	01-L_Water [0...350C]
6.6 Defining temperature	Tdef1 25.4981 25.4981 [°C] <input checked="" type="checkbox"/>
6.7 Specific heat capacity	Cp1 4187.919 4187.919 [J/kg/K] <input checked="" type="checkbox"/>

Working fluid 2	13-L_SAE 10W [0...100C]
Defining temperature	Tdef2 80 80 [°C] <input checked="" type="checkbox"/>
Specific heat capacity	Cp2 2132 2132 [J/kg/K] <input checked="" type="checkbox"/>

6.8 Calculation and working fluid parameters

6.9 Mass flow rate	m1' 0.25 0.25 [kg/s]
6.10 Inlet temperature	T1in 20 20 [°C]
6.11 Outlet temperature	T1out 30.9962 30.9962 [°C]
6.12 Temperature difference	dT1,ΔT1 10.9962 25.4981 [°C]
6.13 Heat flow rate	Q1 11.513 [kW]
6.14 Calculation of Logarithmic Mean Temperature Difference (LMTD)	
6.15 Heat capacity rate	C1,C2 1046.98 319.8 [W/K]
6.16 Coefficients R, P	R, P 0.30545 0.461538 [~]
6.17 LMTD Correction factor	ε 1 1 [~] <input checked="" type="checkbox"/>
6.18 Logarithmic Mean Temperature Difference (LMTD)	ΔT' -50.9389 [°C]

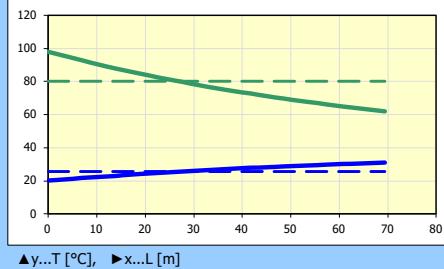
Calculation and working fluid parameters

Mass flow rate	m2' 0.15 0.15 [kg/s]
Inlet temperature	T2in 98 98 [°C]
Outlet temperature	T2out 62 62 [°C]
Swap	Temperature difference dT2,ΔT2 -36 80 [°C]
Heat flow rate	Q2 -11.513 [kW]

6.19 Selection and calculation of Heat exchanger parameters

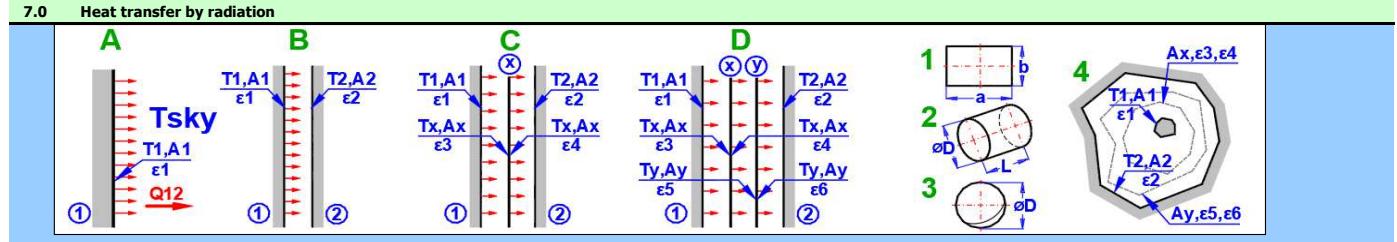
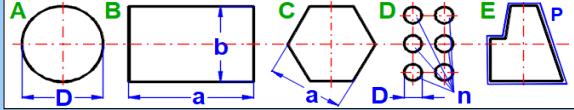
6.20 Required tube length of the exchanger	B. Tubular (tube length)
6.21 Heat transfer coefficient (cylinder)	Ucyl 3.253179 3.253179 [W/m/K] <input checked="" type="checkbox"/>
6.22 Pipe length	L 69.47414526 [m] <input checked="" type="checkbox"/>
6.23 Calculation of outlet temperature depending on tube length	
6.24 Pipe length	L 0.5 [m]
6.25 Outlet temperature	T1out, T2out 20.12078 97.60459 [°C]
6.26 Transfer calculated values	

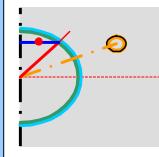
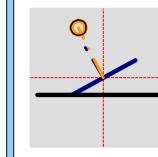
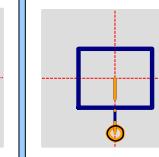
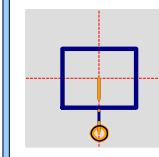
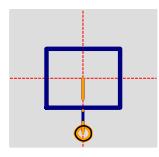
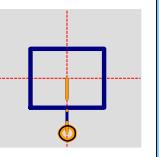
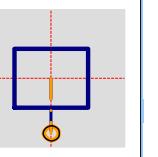
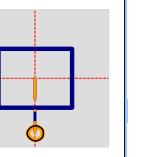
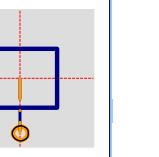
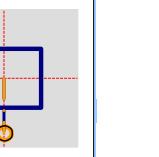
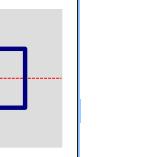
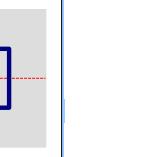
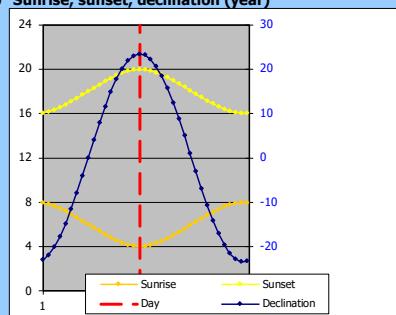
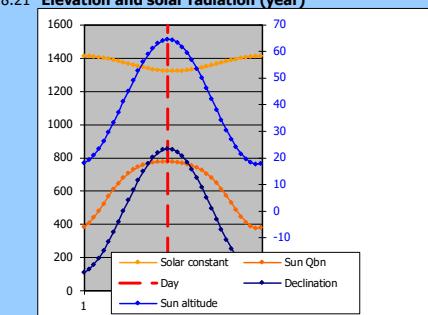
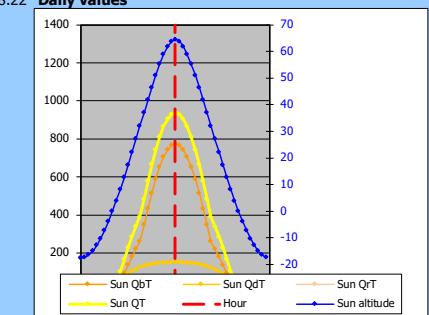
6.15a Temperature profiles



6.27 Conversion of tube length to area

6.28 Tube cross-section	D. Pipe cross-section ... circle
6.29 Pipe length	L 69.47415 69.47415 [m] <input checked="" type="checkbox"/>
6.30 Inner diameter of the pipe	D 0.3 0.3 [mm] <input checked="" type="checkbox"/>
6.31 Number of pipes	n 1 1 [~] <input checked="" type="checkbox"/>
6.32 Heat transfer area	A 0.065477839 [m²] <input checked="" type="checkbox"/>
6.33 Determination of heat transfer coefficient with fouling	
6.34 U - Clean surface	Uc 41.42077 41.42077 [W/m²/K] <input checked="" type="checkbox"/>
6.35 Fouling factor	Rf 1 [m²K/W] <input checked="" type="checkbox"/>
6.36 U - Fouled surface	Ud 0.976427 Δ=-98% [W/m²/K] <input checked="" type="checkbox"/>



7.1 Solved task		B. Two parallel surfaces
7.2 Surface number 1		
7.3 Material group		1. Metals and metal alloys (M)
7.4 Wall material		199-M. Stainless Steel: type 18-8, polished ($\epsilon = 0.10 - 0.19$)
7.5 Wall emissivity		ϵ_1 0.93 0.15 [~] <input checked="" type="checkbox"/>
7.6 Wall temperature		T1 200 27 [°C]
7.7 Area calculation		2. Cylindrical surface ($\pi \cdot D \cdot L$) D1,L1 200 1000 [mm]
7.8 Wall area		A1 0.628319 0.628319 [m^2] <input checked="" type="checkbox"/>
7.9 Shielding foil X		
7.10 Shielding emissivity		ϵ_3, ϵ_4 0.05 0.05 [~]
7.11 Area calculation		Dx,Lx 1900 1000 [mm]
7.12 Foil area		Ax 5.969026 5.969026 [m^2] <input checked="" type="checkbox"/>
7.13 Foil temperature		Tx ~ [°C]
7.14 Heat flux (specific, total)		q12',Q12 2180.757 1370.21 [W/ m^2 ,W]
7.15 Radiation heat transfer coefficient		hr12 12.11532 [W/ m^2 /K]
8.0 Solar radiation		
8.1 Solar radiation		
MM:8 DD:21 HH:18:9		
8.2 Month (1-12), day (1-31)		MM,DD 6 21 5 [m, d] <input checked="" type="checkbox"/>
8.3 Hour (0-24), latitude (± 90)		HH, ζ 12 1 48.9 5 [h, °] <input checked="" type="checkbox"/>
8.4 Surface tilt (0-90), surface azimuth (± 180)		β, γ 30 5 0 5 [°, °] <input checked="" type="checkbox"/>
8.5 Sunrise, sunset, daylight duration		h1,h2,h3 4:0 19:59 15:58 [h:m] 
8.6 Solar elevation (angle above horizon), declination		ϕ, δ 64.54978 23.44978 [°] 
8.7 Solar irradiance (solar constant)		Qon 1322.624 1322.624 [W/ m^2] 
8.8 Altitude		Alt 35 0 [m] 
8.9 Atmospheric pollution coefficient (1.5-6)		Z 5 5 [~] 
8.10 Sun azimuth, sun angle to surface normal		ys,θ 0 4.549783 [°] 
8.11 Radiant power on a defined / perpendicular surf.		QbT,Qbn 775.0822 777.5324 [W/ m^2] 
8.12 Diffuse radiation on a defined / horizontal surfac		QdT,Qd 151.5441 162.4244 [W/ m^2] 
8.13 Ground reflectivity (albedo)		Rhog 0.2 0.2 [~] 
8.14 Reflected solar radiation on a given surface		QrT 11.58216 [W/ m^2] 
8.15 Surface area		As 1 [m^2] 
8.16 Total solar irradiance (QbT+QdT+QrT)		QT,QTs 938.2084 938.2084 [W/ m^2 ,W] 
8.17 Energy conversion efficiency		Eff 100 100 % 
8.18 Surface power		Q,Qs 938.2084 938.2084 [W/ m^2 ,W] 
8.19 Daily surface energy		Pw,Pws 8.019433 8.019433 [kWh/ m^2 ,kWh] 
8.20 Sunrise, sunset, declination (year)		
 <p>X:Day, yL:Hour, yR:Angle</p>		
8.21 Elevation and solar radiation (year)		
 <p>X:Day, yL:Power, yR:Angle</p>		
8.22 Daily values		
 <p>X:Hour, yL:Power, yR:Angle</p>		