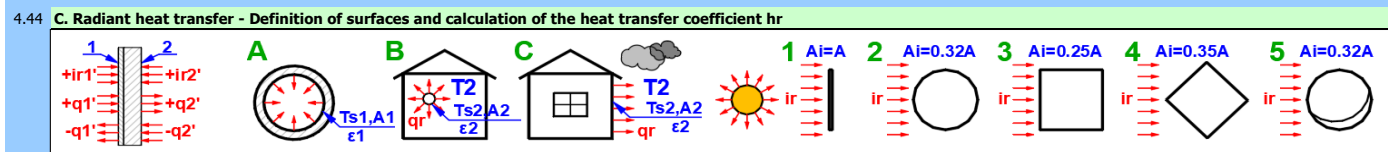


4.20	Coefficient of volumetric expansion	β	3.38E-03	[1/K]	Coefficient of volumetric expansion	β	3.65E-03	[1/K]		
4.21	Kinematic viscosity	ν	15.42656	[mm ² /s]	Kinematic viscosity	ν	13.44042	[mm ² /s]		
4.22	Flow type: A-Forced convection, B-Natural convection				Flow type: A-Forced convection, B-Natural convection					
4.23	B - 14. Vertical surface (Heat Transfer Appl. for the PE) [1e3<Ra<1e13]				A - 13. Flow across a plate (Heat Transfer Appl. for the PE) [Re<1e7, 0.1<Pr<1e3 (Turb.0.6<Pr<60)]					
4.24	Flow velocity, Flow rate	$v1, m1'$	0.001	0.014861	[m/s, kg/s]	Flow velocity, Flow rate	$v2, m2'$	2	32.12081	[m/s, kg/s]
4.25	Dimension according to the figure	a	2500	1000	[mm]	Dimension according to the figure	a	2500	2500	[mm]
4.26	Dimension according to the figure	L	5000	1000	[mm]	Dimension according to the figure	L	5000	5000	[mm]
4.27	Dimension according to the figure		0	0		Dimension according to the figure		0	0	
4.28	Dimension according to the figure		0	0		Dimension according to the figure		0	0	
4.29	Finned surface				Finned surface					
4.30	Finned area	At1	12.905		[m ²]	Finned area	At2	114.29		[m ²]
4.31	Fin efficiency	η_{of1}	0.978347	0.978347	[~]	Fin efficiency	η_{of2}	0.408474	0.408474	[~]
4.32	Tube bank				Tube bank					
4.33	Distance between tubes	ST, SL	3183.099	3183.099	[mm]					
4.34	Number of rows / number of columns	m, n	5	5	[~]					
4.35	Number of tubes in the tube bank	N	1	1	[~]					
4.36	Flow velocity between tubes	$v2_{max}$	9.319585	9.319585	[m/s]					
4.37	Heat transfer area inner (left)	A1	12.5	12.5	[m ²]	Heat transfer area outer (right)	A2	12.5	12.5	[m ²]
4.38	Prandtl number	Pr, Prs	0.716095	0.71202	[~]	Prandtl number	Pr, Prs	0.71968	0.72114	[~]
4.39	Reynolds number, Critical Re	Re, Recr	0	1E+09	[~]	Reynolds number, Critical Re	Re, Recr	372012.1	500000	[~]
4.40	Grashof number, Rayleigh number	Gr, Ra	9.52E+09	6.82E+09	[~]	Grashof number, Rayleigh number	Gr, Ra	4.4E+09	3.17E+09	[~]
4.41	Nusselt number, Characteristic dimension	Nu, a	243.6238	2500	[~], [mm]	Nusselt number, Characteristic dimension	Nu, a	362.9727	2500	[~], [mm]
4.42	Convective heat transfer coefficient	hc1	2.511393	2.51128	[W/m ² /K]	Convective heat transfer coefficient	hc2	3.501548	3.501548	[W/m ² /K]
4.43	Heat flux - convection (specific, total)	q_{c1}' , Q_{c1}	10.99051	137.3813	[W/m ² , W]	Heat flux - convection (specific, total)	q_{c2}' , Q_{c2}	4.971476	62.14345	[W/m ² , W]



4.45	1. Surface - Inner (left) side				4.46	2. Surface - Outer (right) side					
4.46	Material group	1. Metals and metal alloys (M)			4.46	Material group	7. Minerals, glass (N)				
4.47	Wall material	032-B. Granite: Rough ($\epsilon = 0.9$)			4.47	Wall material	045-B. Plaster: Rough ($\epsilon = 0.91$)				
4.48	Emissivity	ϵ_1	0.900	0.900	[~]	4.48	Emissivity	ϵ_2	0.910	0.910	[~]
4.49	1. Radiation - From inner (left) side				4.49	2. Radiation - From outer (right) side					
4.50	Heat radiation into space	A. Not used (closed space..)			4.50	Heat radiation into space	B. General space radiation				
4.51	Radiating area, inner (left)	Ar1	12.5	12.5	[m ²]	4.51	Radiating area, outer (right)	Ar2	12.5	12.5	[m ²]
4.52	Radiation heat transfer coefficient	hr1	0		[W/m ² /K]	4.52	Radiation heat transfer coefficient	hr2	4.23937		[W/m ² /K]
4.53	Heat flux - radiation (specific, total)	q_{r1}' , Q_{r1}	0	0	[W/m ² , W]	4.53	Heat flux - radiation (specific, total)	q_{r2}' , Q_{r2}	6.019031	75.23788	[W/m ² , W]
4.54	1. Irradiation - On inner (left) side				4.54	2. Irradiation - On outer (right) side					
4.55	Incident radiation intensity	i_{r1}'	0	* 1	[W/m ²]	4.55	Incident radiation intensity	i_{r2}'	0	* ϵ	[W/m ²]
4.56	Irradiated area size	Ai1	1.25E+01	1=A	[m ²]	4.56	Irradiated area size	Ai2	12.5	1=A	[m ²]
4.57	Radiation heat transfer coefficient	hi1	0		[W/m ² /K]	4.57	Radiation heat transfer coefficient	hi2	0		[W/m ² /K]
4.58	Heat flux - irradiation ($\emptyset$ specific, total)	q_{i1}' , Q_{i1}	0	0	[W/m ² , W]	4.58	Heat flux - irradiation ($\emptyset$ specific, total)	q_{i2}' , Q_{i2}	0	0	[W/m ² , W]

4.59	Heat transfer results				4.59	Heat transfer results					
4.60	Convection + radiation + irradiation				4.60	Convection + radiation + irradiation					
4.61	Heat transfer coefficient	hc1	2.511393		[W/m ² /K]	4.61	Heat transfer coefficient	hc2	7.740919		[W/m ² /K]
4.62	Heat flux - total (specific, total)	q_{cr1}' , Q_{cr1}	10.99051	137.3813	[W/m ² , W]	4.62	Heat flux - total (specific, total)	q_{cr2}' , Q_{cr2}	10.99051	137.3813	[W/m ² , W]
4.63	Overall heat transfer coefficient U, Overall thermal resistance R				4.63	Overall heat transfer coefficient U, Overall thermal resistance R					
4.64	Inner (left) surface	U1, R1	0.43962	2.274691	[W/m ² /K, m ² K/W]	4.64	Outer (right) surface	U2, R2	0.43962	2.274691	[W/m ² /K]
4.65	Cylindrical wall	Ucyl1, Rcyl1	1.099051	0.909876	[W/m ² /K, m.K/W]	4.65	Cylindrical wall	Ucyl2, Rcyl2	1.099051	0.909876	[W/m ² /K]
4.66	Spherical wall	Usp1, Rsp1	5.495253	0.181975	[W/K, K/W]	4.66	Spherical wall	Usp2, Rsp2	5.495253	0.181975	[W/K]
4.67	Wall thermal resistance (wall only)	Rwall	1.747321		[m ² K/W]	4.67	Wall thermal resistance (wall only)	Rwall	1.747321		[m ² K/W]
4.68	Heating / cooling of the working medium				4.68	Heating / cooling of the working medium					
4.69	Flow area	Af1	1.25E+01	12.5	[m ²]	4.69	Flow area	Af2	1.25E+01	12.5	[m ²]
4.70	Density	Rho	1.180158	1.180158	[kg/m ³]	4.70	Density	Rho	1.288172	1.288172	[kg/m ³]
4.71	Specific heat capacity	Cp	1006.314	1006.314	[J/kg/K]	4.71	Specific heat capacity	Cp	1005.064	1005.064	[J/kg/K]
4.72	Flow rate	m'	0.014752		[kg/s]	4.72	Flow rate	m'	90000		[m ³ /h]
4.73	Inlet / Outlet temperature	Tin1, Tout1	25	17.266	[°C]	4.73	Inlet / Outlet temperature	Tin2, Tout2	0	0.003547	[°C]
4.74	Heat flux - mean (specific, total)	q_{s1}' , Q_{s1}	9.184974	114.8122	[W/m ² , W]	4.74	Heat flux - mean (specific, total)	q_{s2}' , Q_{s2}	9.184974	114.8122	[W/m ² , W]

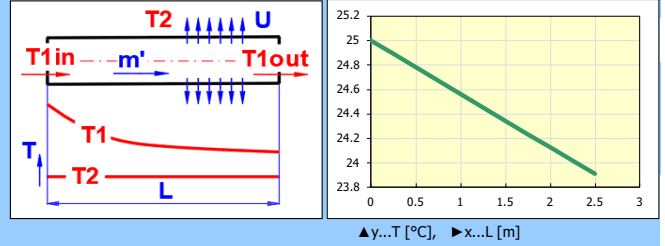
4.75	Saving the wall heat transfer solution				4.80	Loading a wall heat transfer solution			
4.76	Solution name				4.81	Solution selection	16	Date:	20250808 - 17:04:31
4.77	Structural wall (brick)				4.82	Structural wall (brick) [T1=25 (Air) => T2=0 (Air); U1=0.44; q1=11; q2=11]			
4.78	T1=25 (Air) => [300mm] => T2=0 (Air); U1=0.44; q1=11; q2=11				4.83	T1=25 (Air) => [300mm] => T2=0 (Air); U1=0.44; q1=11; q2=11			
4.79	Structural wall: Plaster, brick, insulation, plaster				4.84	Structural wall: Plaster, brick, insulation, plaster			

4a.0	Definition and calculation of finned wall				
4a.1	1. Fin type - Internal (left) side				
4a.2	Thermal conductivity of fin material	λ	0.7	[W/(m.K)]	
4a.3	Convective heat transfer coefficient	hc1	2.511393	[W/m ² /K]	
4a.4	Wall temperature, medium temperature	Ts1, T1	20.62374	25	[°C]
4a.5	Finned field width	a	50	5000	[mm]
4a.6	Fin profile	A. Rectangle			
4a.7	Fin thickness	t	38	38	[mm]
4a.8	Fin height	hf	100	100	[mm]
4a.1	2. Fin type - External (right) side				
4a.2	Thermal conductivity of fin material	λ	0.7	[W/(m.K)]	
4a.3	Convective heat transfer coefficient	hc2	3.501548	[W/m ² /K]	
4a.4	Wall temperature, medium temperature	Ts2, T2	1.419794	0	[°C]
4a.5	Finned field width	a	5000	5000	[mm]
4a.6	Fin profile	A. Rectangle			
4a.7	Fin thickness	t	3	38	[mm]
4a.8	Fin height	hf	45	100	[mm]

4a.9	Distance between fins (fin pitch)	s	86	86	[mm]	Distance between fins (fin pitch)	s	10.7	100	[mm]
4a.10	Number of fins in the finned field	n	1	≤ 1	[~]	Number of fins in the finned field	n	468	≤ 468	[~]
4a.11	Area of one fin / Total area	Af, At	0.595	12.905	[m²]	Area of one fin / Total area	Af, At	0.2325	114.29	[m²]
4a.12	Parameter x, fin efficiency	x, ηf	1.2614	0.5304	[~]	Parameter x, fin efficiency	x, ηf	1.9302	0.3787	[~]
4a.13	Overall finned surface efficiency	ηof	0.9783		[~]	Overall finned surface efficiency	ηof	0.4085		[~]
4a.14	Heat flux - total (specific, overall)	q1', Q1	10.75253	138.7614	[W/m², W]	Heat flux - total (specific, overall)	q2', Q2	2.03072	232.0909	[W/m², W]

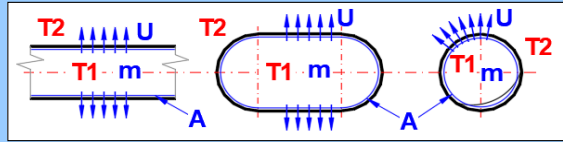
5.0 Longitudinal temperature change in piping, temperature change and cooling time in the tank (ISO 12241)

5.1	Working fluid	01-L. Water	[0...350C]			
5.2	Defining temperature	Tdef	25	25	[°C]	☒
5.3	Specific heat capacity	Cp	4187.655	4187.655	[J/kg/K]	☒
5.4 Calculation of longitudinal temperature change in piping						
5.5	Fluid temperature at pipe inlet	T1in	25	25	[°C]	☒
5.6	Ambient temperature	T2	0	0	[°C]	
5.7	Mass flow rate through the piping	m'	0.014752	0.014752	[kg/s]	
5.8	Heat transfer coefficient (cylinder)	Ucyl	1.099051	1.099051	[W/m²/K]	
5.9	Distance from the beginning of the pipe	L	2.5	2.5	[m]	☒
5.10	Fluid temperature at point L	T1out	23.9124		[°C]	
5.11	Power loss (-) / gain (+)	Pw	-0.067185479		[kW]	

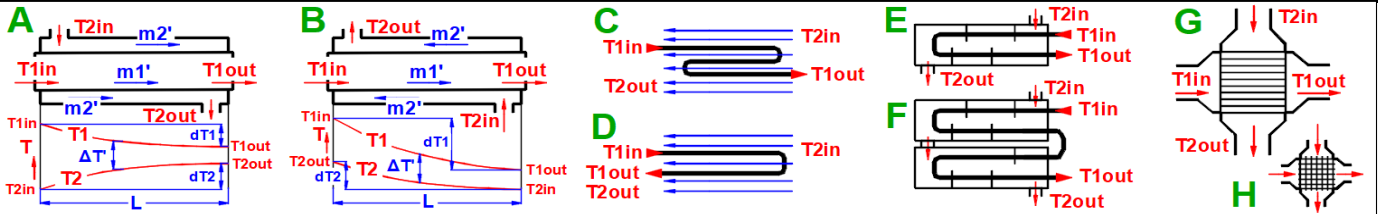


5.12 Temperature change and cooling time in pipes and tanks

5.13	Initial fluid temperature	T1s	25	25	[°C]
5.14	Final fluid temperature	T1e	20	0~25	[°C]
5.15	Ambient temperature	T2	0	0	[°C]
5.16	Mass of fluid in the tank	m	0.85		[kg]
5.17	Heat transfer coefficient (area)	U	0.43962	0.43962	[W/m²/K]
5.18	Internal area of the tank or pipe	A	12.5	12.5	[m²]
5.19	Time for cooling / heating	Time	144.54		[s]
5.20	Time for cooling / heating	Time	0-0:2:24.54		[d-h-m:s]
5.21	Energy lost (-) / gained (+)	E	-0.004943763		[kWh]



6.0 Heat exchangers



6.1	Heat exchanger type	A. Parallel flow heat exchanger (tube-within-a-tube)
6.2	Load parameters (select from saved wall definitions / current definition)	
6.3	List of defined walls	8
6.4	Load current parameters from section 4.0 (wall definition)	

6.5	Working fluid 1	01-L. Water [0...350C]				
6.6	Defining temperature	Tdef1	25.4981	25.4981	[°C]	☒
6.7	Specific heat capacity	Cp1	4187.919	4187.919	[J/kg/K]	☒
6.8 Calculation and working fluid parameters						
6.9	Mass flow rate	m1'	0.25	0.25	[kg/s]	
6.10	Inlet temperature	T1in	20	20	[°C]	
6.11	Outlet temperature	T1out	30.9962	30.9962	[°C]	
6.12	Temperature difference	dT1,ΔT1	10.9962	25.4981	[°C]	
6.13	Heat flow rate	Q1	11.513		[kW]	

Working fluid 2		13-L. SAE 10W		[0...100C]		▼	
Defining temperature	Tdef2	80	80	[°C]		☑	
Specific heat capacity	Cp2	2132	2132	[J/kg/K]		☑	
Calculation and working fluid parameters							
Mass flow rate	m2'	0.15	0.15	[kg/s]			
Inlet temperature	T2in	98	98	[°C]			
Outlet temperature	T2out	62	62	[°C]			
Temperature difference	dT2,ΔT2	-36	80	[°C]			
Heat flow rate	Q2	-11.513		[kW]			

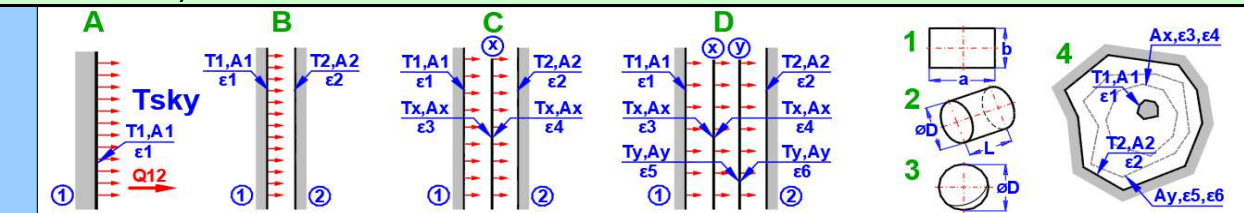
6.14	Calculation of Logarithmic Mean Temperature Difference (LMTD)				
6.15	Heat capacity rate	C1, C2	1046.98	319.8	[W/K]
6.16	Coefficients R, P	R, P	0.30545	0.461538	[~]
6.17	LMTD Correction factor	ε	1	1	[~]
6.18	Logarithmic Mean Temperature Difference (LMTD)	ΔT'	-50.9389		[°C]

6.19	Selection and calculation of Heat exchanger parameter	B. Tubular (tube length)
6.20	<i>Required tube length of the exchanger</i>	

6.23	Calculation of outlet temperature depending on tube length				
6.24	Pipe length	L	0.5		[m]
6.25	Outlet temperature	T1out, T2out	20.12078	97.60459	[°C]
6.26	Transfer calculated values				
6.27	Conversion of tube length to area				
6.28	Tube cross-section	D. Pipe cross-section ... circle			
6.29	Pipe length	L	69.47415	69.47415	[m]
6.30	Inner diameter of the pipe	D	0.3	0.3	[mm]
6.31	Number of pipes	n	1	1	[~]
6.32	Heat transfer area	A	0.065477839		[m²]

6.33	Determination of heat transfer coefficient with fouling				
6.34	U - Clean surface	Uc	41.42077	41.42077	[W/m²/K]
6.35	Fouling factor	Rf	1		[m²K/W]
6.36	U - Fouled surface	Ud	0.976427	Δ=-98%	[W/m²/K]

7.0 Heat transfer by radiation



7.1 Solved task		B. Two parallel surfaces							7.2 Surface number 1		= > > Surface number 2				
7.3 Material group		1. Metals and metal alloys (M)							7.3 Material group		1. Metals and metal alloys (M)				
7.4 Wall material		199-M. Stainless Steel: type 18-8, polished ($\epsilon = 0.10 - 0.19$)							7.4 Wall material		199-M. Stainless Steel: type 18-8, polished ($\epsilon = 0.10 - 0.19$)				
7.5 Wall emissivity		ϵ_1	0.93	0.15	[~]	☒			7.5 Wall emissivity		ϵ_2	0.736	0.15	[~]	☒
7.6 Wall temperature		T1	200	27	[°C]				7.6 Wall temperature		T2	20		[°C]	
7.7 Area calculation		2. Cylindrical surface ($\pi r^2 D^* L$)						7.7 Area calculation		D2,L2		2000	1000	[mm]	
7.8 Wall area		A1	0.628319	0.628319	[m²]	☒			7.8 Wall area		A2	6.283185	6.283185	[m²]	☒
7.9 Shielding foil X									7.9 Shielding foil Y						
7.10 Shielding emissivity		ϵ_3, ϵ_4	0.05	0.05	[~]				7.10 Shielding emissivity		ϵ_5, ϵ_6	0.33	0.6	[~]	
7.11 Area calculation		D_x, L_x	1900	1000	[mm]				7.11 Area calculation		D_y, L_y	1000	1000	[mm]	
7.12 Foil area		A_x	5.969026	5.969026	[m²]	☒			7.12 Foil area		A_y	3.141593	3.141593	[m²]	☒
7.13 Foil temperature		T_x			[°C]				7.13 Foil temperature		T_y			[°C]	
7.14 Heat flux (specific, total)		q_{12}', Q_{12}	2180.757	1370.21	[W/m², W]				7.14 Heat flux (specific, total)		q_{21}', Q_{21}	-218.0757	-1370.21	[W/m², W]	
7.15 Radiation heat transfer coefficient		hr_{12}	12.11532		[W/m²/K]				7.15 Radiation heat transfer coefficient		hr_{21}	1.211532		[W/m²/K]	